

Hydrodechlorination of Trichloromethane to Higher Hydrocarbons over Pd/SiO₂ Catalyst

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Pd/SiO₂ catalyzed C–C bond formation selectively to give C₂–C₇ hydrocarbons in the hydrodechlorination of CHCl₃. The produced hydrocarbons followed well the Schultz–Flory distribution, indicating that the hydrocarbons were formed via polymerization of surface C₁ species such as methylene group.

Catalytic hydrodechlorination of chlorine-containing compounds has been studied extensively in recent years to convert them into environmentally benign and more useful products.^{1–6} It has been known that C–C bond formation takes place during the hydrodechlorination of some compounds.^{2–6} Over Ru/SiO₂, CCl₂F–CClF₂ is dehydrodechlorinated into CClF=CF₂² while CCl₃–CF₃ is dehydrodechlorinatively dimerized to form C₄ selectively (90% selectivity).³ The hydrodechlorination of CCl₄ over Pd/C and Pd/TiO₂ yields hydrocarbons having chain length up to C₅⁴ and that of CH₂Cl₂ over Pd/Al₂O₃ yields Cl–H replacement products, CH₄ and CH₃Cl, selectively.⁷ Discrepancy is found in the reports on the hydrodechlorination of CCl₂F₂ over Pd/C. Wiersma et al.⁵ have reported the selective Cl–H replacement to CH₂F₂ and Kulkarni et al.⁶ do the oligomerization to give CH₂=CF₂, CH₂=CH₂, and C₃, although their reaction conditions are not very different. Recently, we found selective formation of hydrocarbons in the hydrodechlorination of CHCl₃ over silica-supported Pd catalysts. The results are reported here.

Various silica-supported noble metal catalysts were prepared by an ion-exchange method with an ammoniacal solution of [Ru(NH₃)₆]Cl₃, [Rh(NH₃)₆]Cl₃, [Pd(NH₃)₄]Cl₂, or [Pt(NH₃)₄]Cl₂. After allowing to ion-exchange for one day, the solids were filtered, dried in an oven overnight at 110 °C. Prior to the reaction catalyst was treated in a H₂ stream at 450 °C for 2 h. CHCl₃ (Kanto Chemical) was washed with distilled water to remove ethanol added as stabilizer and then dried with CaCl₂.

The reaction of CHCl₃ with hydrogen was carried out in a conventional flow-type reaction system with a Pyrex glass reactor under atmospheric pressure. The reaction conditions were as follows: temperature, 200 °C; feed composition (molar ratio), Ar : H₂ : CHCl₃ = 19.5 : 9.5 : 1; total flow rate, 60 cm³ min⁻¹; catalyst amount, 0.100 g. The feed and effluent gases were analyzed by a gas chromatograph (Shimadzu GC-9A) equipped with a thermal conductivity detector and a flame ionization detector using a Gaskuropack 54 column (GL Sciences). The products were identified with a GC–MS (Hitachi M-80B) using the same column.

The results of hydrodechlorination of CHCl₃ over silica-supported noble metal catalysts are shown in Table 1, where the data obtained at 3 h on stream were summarized. Among the catalysts employed, Pd/SiO₂ was most active and the activity did not change appreciably with time on stream (92.2% conversion at 6 h on stream). The products were C₁–C₇ hydrocarbons for the most part and the Cl–H replacement product, CH₂Cl₂,

Table 1. Hydrodechlorination of trichloromethane over silica-supported noble metal catalysts at 200 °C

	Catalyst ^a			
	Pd (0.50)	Pt (0.92)	Rh (0.48)	Ru (0.47)
Conversion / %	93.9	89.9	6.5	1.4
Selectivity / %				
CH ₂ Cl ₂	0.5	28.8	13.5	9.6
Hydrocarbon				
C ₁	51.7	71.1	25.6	1.9
C ₂	31.1	tr.	3.3	0.6
C ₃	10.2	-	4.0	0.6
C ₄	4.4	-	2.7	tr.
C ₅	1.4	-	2.0	-
C ₆	0.5	-	0.9	-
C ₇	0.2	-	1.0	-

^aThe number in the parenthesis indicates the amount of metal loading (wt%) which corresponds to 47 μmol g-cat.⁻¹ for all catalysts.

was formed at the selectivity as low as 0.05%. The hydrocarbons produced were alkanes and the ratio of branched to normal for C₄, C₅, C₆, and C₇ was 0.16, 0.70, 0.97, and 1.3, respectively. Pt/SiO₂ also showed high activity for the reaction giving Cl–H replacement products, CH₄ and CH₂Cl₂, mainly but the activity decreased with time on stream gradually (77.4% conversion at 6 h on stream). Over Rh/SiO₂, hydrocarbons are formed at relatively high selectivity but the value of conversion was much lower than that over Pd/SiO₂ and decreased to 2.1% at 6 h on stream. Ru/SiO₂ catalyzed the dimerization of CCl₃–CF₃ reported previously,³ but the catalytic activity for this reaction was very poor. Over Rh and Ru catalysts, the total selectivity of gaseous products was considerably low suggesting carbon deposition on the catalyst surface, and more than half of C₂₊ hydrocarbons produced were alkenes. Chlorine coverage on the metal surface under hydrodechlorination conditions increases in the order of Pd < Rh < Ru;^{5,6} that is, the coverage of dissociatively adsorbed hydrogen might decrease in the same order. It seems that insufficiency of adsorbed hydrogen on Rh and Ru causes the conversion of adsorbed C₁ species into alkenes and carbonaceous.

Figure 1 presents the effect of reaction temperature on the hydrodechlorination of CHCl₃ over Pd/SiO₂. The values of conversion and selectivity were obtained after the reaction reached its steady state at each temperature. When the reaction temperature increased from 100 °C to 225 °C, the conversion of CHCl₃ increased from 1.85% to 98.8% and the Cl–H replaced product CH₂Cl₂ was always formed as minor products decreasing its selectivity from 1.7 to 0.5%. The selectivity for CH₄ decreased and those for C₂₊ alkanes increased with reaction temperature. In a supplemental study, the contact time did not give much influence to the product distribution. The result indicates that the carbon chain-growth reaction does not result

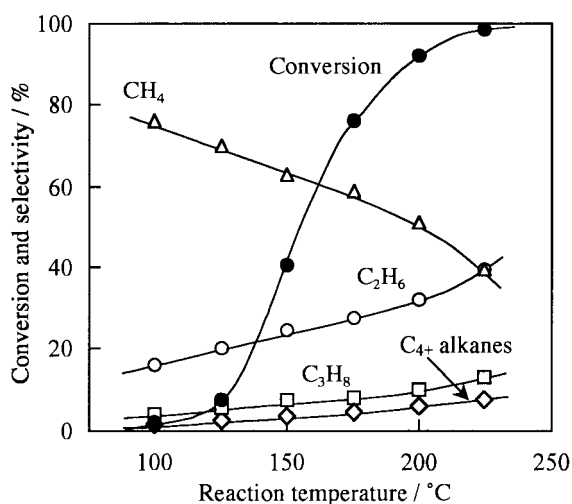


Figure 1. Hydrodechlorination of trichloromethane over 0.50 wt% Pd/SiO₂ at various temperatures.

from the consecutive C–C bond formation through the readorption of desorbed molecules.

Figure 2 shows the Schultz–Flory plots for compositions of hydrocarbons formed over Pd/SiO₂ at various temperatures. The Schultz–Flory distribution is expressed by eq (1); where C_n is the mole fraction of the hydrocarbon with n_c carbon atoms and α represents the probability of chain-growth.⁸

$$\ln(C_n) = n_c \ln \alpha + \ln(C_1/\alpha) \quad (1)$$

As seen in Figure 2, the composition of hydrocarbons formed at every temperature followed eq (1) at the correlation coefficient more than 0.994. This means that higher hydrocarbons are formed through the polymerization of surface C₁ species like a Fischer–Tropsch reaction. The probability of chain-growth (α) calculated from the slope of each line in Figure 2, was increased from 0.15 (100 °C) to 0.28 (200 °C) with reaction

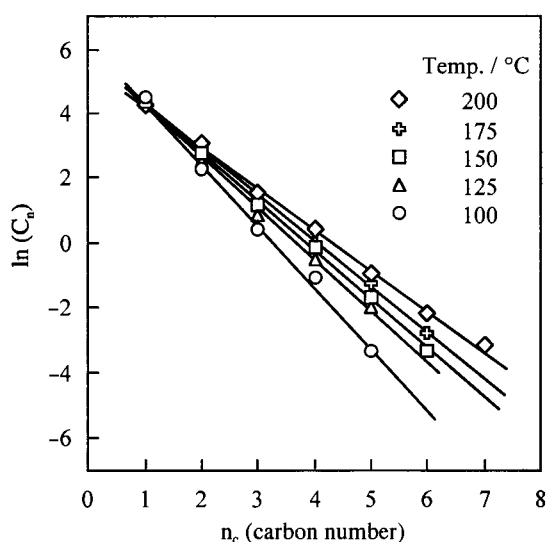


Figure 2. Shultz–Flory plots for hydrocarbons formed in the hydrodechlorination of trichloromethane over 0.50 wt% Pd/SiO₂.

temperature. Although the surface C₁ species is not well understood yet at this stage of investigation, the C₁ species is considered to be methylene group (CH₂=) formed by dechlorination/hydrogenation of adsorbed CHCl₃, because the chlorine containing C₂₊ hydrocarbon is not detected in the products.

C₂₊ hydrocarbons were not produced in the hydrodechlorination of CH₂Cl₂ and those including alkenes were formed in the reaction of CCl₄ over Pd catalysts. The difference of selectivity to oligomerization products is explainable by the reactivity of chloromethanes. The reactivity namely the tendency to C–Cl bond cleavage increases remarkably with the number of chlorine atoms in it (CH₂Cl₂ < CHCl₃ < CCl₄).⁹ It is likely that CH₂Cl₂ adsorbs dissociatively on Pd at the lower coverage because of its lower reactivity, leading to the higher coverage of adsorbed hydrogen, and the surface C₁ species are attacked by adsorbed hydrogen preferentially to form Cl–H replacement products, CH₄ and CH₃Cl. The high reactivity of CCl₄ seems to cause the higher coverage of C₁ species and chlorine, resulting in the coupling into alkenes and marked deactivation by carbon deposit because of the shortage of adsorbed hydrogen.

The selective hydrocarbon formation from CHCl₃ we report here is expected to be a potential process for a methane conversion into hydrocarbons under mild condition, since CH₄ is converted easily to CHCl₃ by the reaction with Cl₂ and HCl formed can be oxidized back to Cl₂.

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